## Pentose Acting as a Sacrificial Multielectron Source in Photocatalytic Hydrogen Evolution from Water by Pt-doped  $TiO<sub>2</sub>$

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Photocatalytic reaction was performed by irradiation of Pt-doped  $TiO<sub>2</sub>$  in an aqueous solution of xylose acting as a sacrificial reagent to evolve hydrogen, whose amounts reached 8.6 equivalents to the xylose used.

Biofuel has been receiving a great amount of interest from the standpoint of utilization as a renewable resource.<sup>1</sup> However, commercially available bio-ethanol has been prepared from the starch of maize, sugarcane, and sugar sorghum, which are in competition with food sources for human consumption.<sup>2</sup> Therefore, we are interested in herbaceous cellulosic biomass such as napier grass and silver grass which is not in competition with food sources.<sup>3</sup> Recently we have reported the production of bioethanol from napier grass (Pennisetum purpureum Schumach) through enzymatic saccharification and fermentation with yeast (Saccharomyces cerevisiae). In this process, 8.8 g of ethanol was produced from 100 g of napier grass containing 44 g of cellulosic components.<sup>4</sup> Thus, ethanol yield was low because of high content of hemicellulose  $(20-35 \text{ wt})$  composed of pentose, which cannot be fermented to ethanol by yeast. Therefore, the transformation of pentose to biofuel is highly desirable in the lignocellulosic biomass conversion (Scheme 1).

The first approach of photocatalytic conversion from carbohydrate to hydrogen has been reported by Kawai et al. 5 Recently, it was reported that Pt-doped TiO<sub>2</sub> (Pt/TiO<sub>2</sub>) can catalyze photochemical H<sub>2</sub> evolution using a hexose as a sacrificial reagent according to eq 1.<sup>6</sup> Therefore, it is expected that this reaction can be applied to pentose (eq 2). Here, we examined the conversion from pentose to hydrogen by photocatalytic reaction with the  $Pt/TiO<sub>2</sub>$  in order to develop a methodology to produce biofuels from cellulosic materials efficiently.

$$
C_6H_{12}O_6 + 6H_2O \xrightarrow{hV} 6CO_2 + 12H_2
$$
 (1)

$$
C_5H_{10}O_5 + 5H_2O \quad \frac{h\nu}{Pt/TiO_2} \quad 5CO_2 + 10H_2 \tag{2}
$$



Scheme 1. Biofuels production from lignocellulose.

The photocatalytic  $H_2$  evolution was performed using a Pt/ TiO<sub>2</sub> catalyst which contained 2 wt % of Pt.<sup>7</sup> The Pt/TiO<sub>2</sub> and an aqueous solution of xylose  $(1a, C_5H_{10}O_5)$  were introduced to a reaction vessel. The volume of reaction solution was adjusted to 150 mL with water. A high-pressure mercury lamp (100 W, UVL-100HA, Riko, Japan) was inserted into the reaction vessel which was connected to a measuring cylinder. The evolved gas was collected by a measuring cylinder and was analyzed by GLC.<sup>8</sup> The reaction vessel was purged by  $N_2$  gas and was set in a water bath to keep at a constant temperature (usually  $20^{\circ}$ C).

Irradiation was performed with a high-pressure mercury lamp under vigorous stirring with a magnetic stirrer until the gas evolution stopped. In order to efficiently irradiate the  $Pt/TiO<sub>2</sub>$ suspended in solution, the amount of the  $Pt/TiO<sub>2</sub>$  was optimized using  $1a$  (150 mg) (Table 1, Runs 1-4). When 100 mg of the  $Pt/TiO<sub>2</sub>$  was used in an aqueous solution (150 mL), the largest amount of  $H_2$  was evolved. In the absence of the sacrificial reagent, the hydrogen evolution from water by irradiation of Pt/  $TiO<sub>2</sub>$  was small (Run 5). The photocatalytic reaction was performed for an aqueous suspension (150 mL) of the  $Pt/TiO<sub>2</sub>$  $(100 \text{ mg})$  with varying amounts of 1a  $(38-188 \text{ mg})$  (Runs 6-9). The molar ratio of the evolved  $H_2$  to 1a is plotted against the weight ratio of 1a to the catalyst in Figure 1. As 1a/catalyst decreased, the  $H<sub>2</sub>/1a$  values increased. The intercept of the plots represents the limiting quantity of hydrogen (N) obtained from one mole of 1a. The N value was 8.6 and did not reach 10 which is the maximum value  $(N_{\text{max}})$  when pentose will be completely decomposed according to eq 2. This suggested that the complete decomposition of  $1a$  into  $CO<sub>2</sub>$  and water did not occur. Therefore, the decomposition procedure of 1a was examined.

Charge separation of  $TiO<sub>2</sub>$  by photoexcitation is well-known to be responsible for the initiation step of the present photocatalytic reaction.<sup>9</sup> The electron reduced water to generate  $H_2$ (eq 3). The hole  $(h<sup>+</sup>)$  oxidizes  $HO<sup>-</sup>$  rather than 1, because of the low concentration of 1 (eq 4).

$$
\text{TiO}_2 \xrightarrow{4 hV} \text{4e}^{\cdot} + 4h^{\cdot} \begin{cases} 4e^{\cdot} + 4H_2O \longrightarrow 2H_2 + 4HO^{\cdot} \qquad (3) \\ 4h^{\cdot} + 4HO^{\cdot} \longrightarrow 4HO^{\bullet} \qquad (4) \end{cases}
$$

The resulting free HO• radical reacted with 1. Fu et al. have postulated a mechanism that the  $h<sup>+</sup>$  oxidizes directly with the alcohol moiety of glucose  $(1b)$ .<sup>6</sup> When the photocatalytic hydrogen evolution was performed using arabitol (1c) as a sacrificial reagent, the hydrogen evolutions were faster than in the case of 1a. Moreover, the ratio of  $H_2$  to  $CO_2$  was constant at 2.5–3.0 even at low conversion, although the ratio of  $H_2$  to  $CO<sub>2</sub>$  exceeded over 2.0 for stoichiometric values, due to the dissolution of  $CO<sub>2</sub>$  into the aqueous reaction solution. Judging

**Table 1.** The photocatalytic  $H_2$  evolution from water using the saccharides 1 as a sacrificial reagent<sup>a</sup>

N <sub>o</sub>	$1/mg^b$		Catalyst /mg	Irradiation time/h <sup>c</sup>	Gas volume/mL			Molar ratio			$N^{\rm f}$
					H <sub>2</sub>	CO <sub>2</sub>	Total <sup>d</sup>	$H_2/1$	$H_2/CO_2$	$N_{\rm max}$ <sup>e</sup>	
	1a $(C_5H_{10}O_5)$	150	75	12	94	47	173	4.2	2.0		
2	1a	150	100	12	111	34	208	5.0	3.3		
3	1a	150	125	12	97	30	182	4.4	3.3		
$\overline{4}$	1a	150	150	12	85	26	165	3.8	3.3		
5	none	$\mathbf{0}$	100	$\overline{4}$	9	$\boldsymbol{0}$	8				
6	1a	38	100	13	46	17	73	8.3	2.7		
7	1a	75	100	15	88	29	120	7.9	3.0		
8	1a	113	100	16	124	42	165	7.4	3.0		
9	1a	150	100	20	164	61	210	7.3	2.7	10	8.6
10	1a	188	100	30	187	76	234	6.7	2.5		
11	1b $(C_6H_{12}O_6)$	180	100	41	139	64	225	6.3	2.2	12	9.3
12	1c $(C_5H_{12}O_5)$	152	100	12	108	23	200	4.8	3.3	11	10.7
13	1d $(C_6H_{12}O_7)$	196	100	30	73	32	164	3.3	2.4	11	7.2
14	1e $(C_4H_7O_5^-)$	102	100	6	43	11	102	5.8	3.9	7	5.6
15	1f $(C_3H_8O_3)$	92	100	6	110	30	112	4.9	3.7	7	7.0
16	1g $(C_3H_6O_3)$	90	100	13	105	37	150	4.7	2.8	6	5.8
17	1h $(C_2H_4O_3)$	76	100	46	47	18	93	2.1	2.5	3	2.0
18	1i $(CH_2O)$ <sup>g</sup>	30	100	13	44	18	84	1.8	2.5	2	1.9

<sup>a</sup>After the bubbling with N<sub>2</sub> gas to purge air, an aqueous solution (150 mL) containing varied amounts of 1 and Pt/TiO<sub>2</sub> (the content of Pt was 2 wt%) was irradiated. <sup>b</sup>Saccharides and the related compounds: xylose (1a), glucose (1b), arabitol (1c), gluconic acid (1d), calcium salt of L-theonate (1e), glycerol (1f), glycelaldehyde (1g), glycolic acid (1h), and methanal (1i). The amounts of 1 in mg. <sup>c</sup>Irradiation time to reach the maximum volume of hydrogen. In the cases of Runs  $1-4$ , the irradiation for  $12h$  was fixed.  $d$ The gas volume in mL collected over water by a measuring cylinder. The collected gas was analyzed by GC. The collected gas involved H2,  $CO_2$ ,  $O_2$ , and N<sub>2</sub>.  $\mathcal{C}N_{\text{max}}$  is the maximum hydrogen amounts in mol evolved from the complete transformation of one mole of 1 which was calculated according to eq 5.  ${}^fN$  is the limiting mole of hydrogen obtained from one mole of 1 obtained from the values of the intercept of the plots of H<sub>2</sub>/1a against 1a/catalyst. <sup>g</sup>Since 35% of the aqueous formaldehyde solution contained 7% methanol as a stabilizer, the hydrogen amounts were corrected by the subtraction of hydrogen from methanol.



**Figure 1.** Dependence of  $H_2$ /1a on the 1a/catalyst. Data from Runs  $6-10$  of Table 1. The N value was determined to be 8.6 from the intercept. Reaction conditions:  $[1a] = 38-188$  mg, catalyst: 100 mg, water: 150 mL.

from these results, the free HO• radical underwent hydrogen abstraction from the  $\alpha$ -carbon of alcoholic and formyl groups. It was suggested that the degradation of 1 proceeded by the sequential removal of  $CO<sub>2</sub>$  from the aldehyde group.<sup>10</sup> Therefore, we postulated Scheme 2 as one possible pathway. Formally the reaction of 1 with four equivalents of HO• radical eliminated one mole of  $CO<sub>2</sub>$  and three moles of  $H<sub>2</sub>O$  from 1. At the same

- CO2 - H2O HO HO *n*−2 C O H C OH H H - H2O - H2O HO **1a**; *n* = 5 **1b**; *n* = 6 **1g**; *n* = 3 *n*−2 C O H C OH H C O OH *n*−2 C O H C OH H C O *n*−2 C O H C OH H C O H *n*−2 C HO H C OH H C O H OH *<sup>n</sup>*−<sup>2</sup> C HO H C OH H C O H HO *n*−2 C HO H C OH H C O H H

**Scheme 2.** A possible reaction scheme for the  $CO<sub>2</sub>$  evolution from saccharides 1 which were presented by Fisher form.

time, 2 equivalents of  $H_2$  evolved by the reduction of water with four electrons.

In order to examine the ability of saccharides as an electron source, photocatalytic hydrogen evolutions were performed for saccharides such as 1a, 1b  $(C_6H_{12}O_6)$ , glycelaldehyde (1g,  $C_3H_6O_3$ ), and methanal (1i, CH<sub>2</sub>O) and the related compounds such as 1c, gluconic acid (1d,  $C_6H_{12}O_7$ ), calcium salt of Ltheonate (1e,  $C_4H_7O_5^-$ ), glycerol (1f),<sup>11</sup> and glycolic acid (1h,  $C_2H_4O_3$ ).<sup>12</sup> The maximum hydrogen amounts in mol ( $N_{\text{max}} =$  $0.5m + 2n - k$ ) evolved from the complete transformation of



Figure 2. Plots of the N values vs. the  $N_{\text{max}}$  values of 1: The aldehyde type  $(\bullet)$ , carboxylic type  $(\bullet)$ , and alcohol type  $\circ$  of sacrificial reagents. The line is a line of  $N = N_{\text{max}}$ .

one mole of 1 ( $C_nH_mO_k$ ) can be calculated according to eq 5 and are listed in Table 1.

$$
C_nH_mO_k + (2n - k) H_2O
$$
  
\n
$$
nCO_2 + (0.5m + 2n - k)H_2
$$
 (5)

\n
$$
H = \begin{pmatrix}\n 0 & 0 & 0 & 0 \\
1 & 0 & 0 & 0 \\
0 & 0 & 0 & 0 \\
0 & 0 & 0 & 0 \\
0 & 0 & 0 & 0 \\
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0 & 0 & 0 & 0 \\
0 & 0 & 0 & 0 \\
0 & 0 & 0 &
$$

The  $N$  values of  $1a-1i$  were obtained from the intercept of the plots of  $H<sub>2</sub>/1$  against 1/catalyst similar to Figure 1. Figure 2 shows the plots of the N values against the  $N_{\text{max}}$  values. In the cases of 1c, 1f, 1g, and 1i, the N values laid on a line of  $N = N_{\text{max}}$ , showing that stoichiometric H<sub>2</sub> evolution occurred, as has been reported for  $1f^{11}$  On the other hand, the N values of saccharides with  $n \geq 4$  (1a and 1b) and the carboxylic compounds (1d, 1e, and 1h) deviated from the line. In the decomposition procedure, 1a and 1b would be partially turned to materials not acting as sacrificial reagents. Thus, we found that one mole of pentose results in 8.6 equivalents of  $H_2$  and 4.3 equivalents of  $CO<sub>2</sub>$ , showing that pentose acted as a 17-electrons source to reduce the  $h^+$  generated on TiO<sub>2</sub>.

It has been established that the  $Pt/TiO<sub>2</sub>$ -photocatalytic hydrogen evolution from water using a variety of sacrificial agents has been applied to reforming of alcohols $11,12$  and decomposition of pollutants.<sup>13-15</sup> Here we can show the methodology to produce hydrogen from lignocellulosic biomass. We intend to obtain conversion from napiergrass to hydrogen by the combination of saccharification with cellulase and the hydrogen evolution with the  $Pt/TiO<sub>2</sub>$  catalyst.

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